



# **Thermal Desorption of VHOC Contaminated Soil and Vapor Management at Lucciana, France**

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Aurélien Vandekerckhove

# OVERVIEW

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Company overview &  
technology principle

2

Site description &  
Approach

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TCH design and results

4

Conclusion



# 1 Company overview & technology principle



# HT TODAY – TECHNOLOGY PROVIDER



Own Lab and R&D facility



Based in Brussels (Belgium)  
55 peoples



Worldwide Operations



Own Smart Burners™  
manufacturing facility



25+ Years in Business

# THEY TRUSTED US

RioTintoAlcan







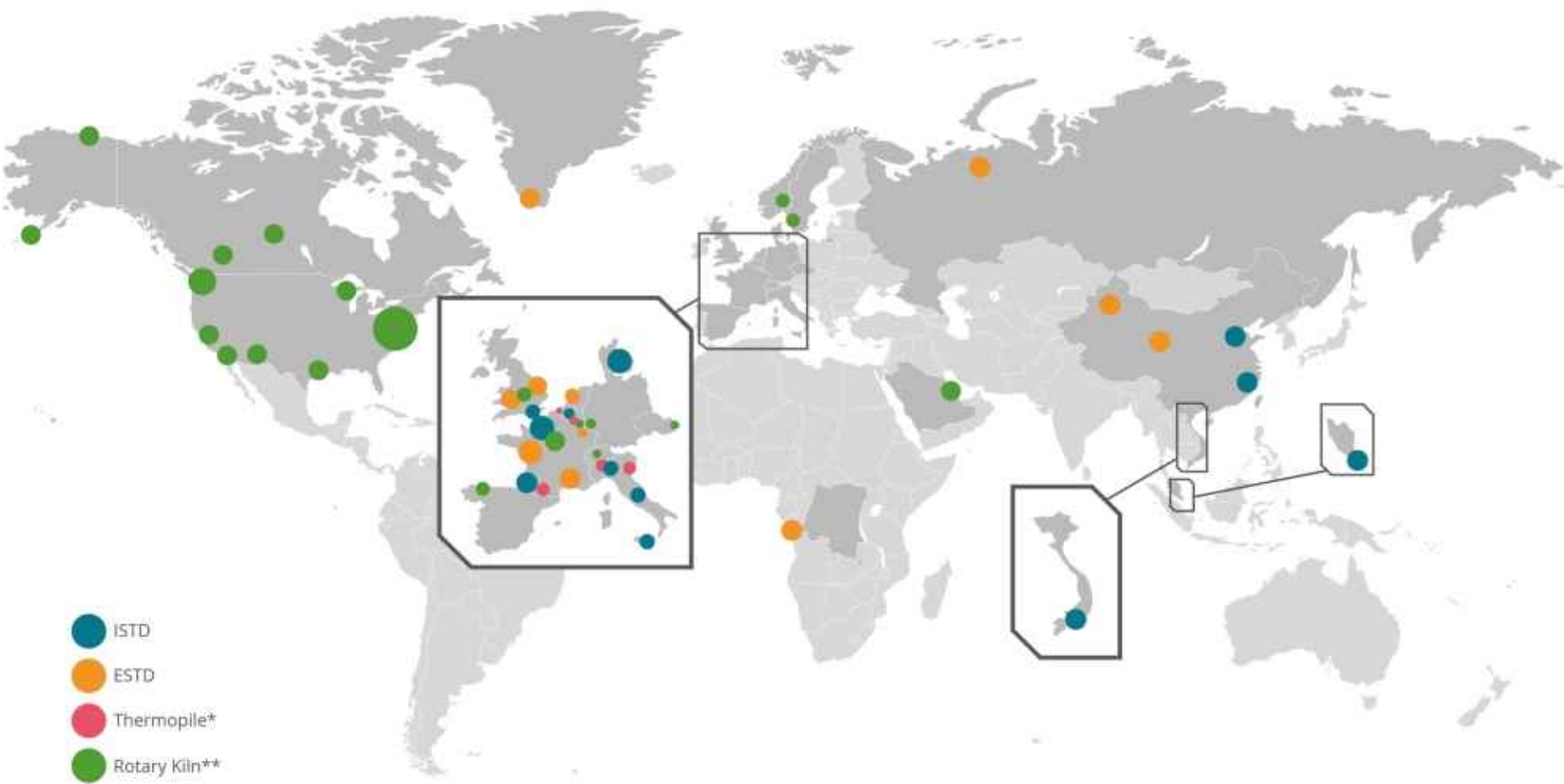






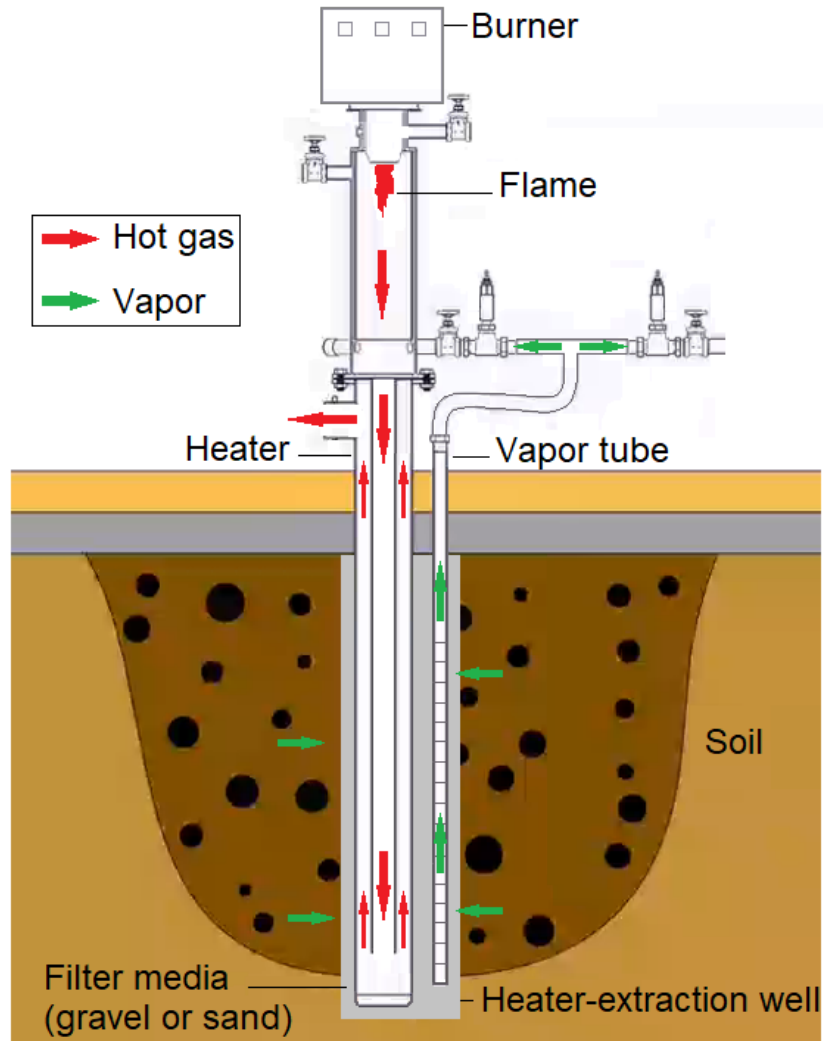


# OPERATIONS WORLDWIDE WITH LOCAL PARTNERS



\*operated by L&C S.A. until 2010  
\*\*operated by TPS Technologies Inc. until 2006

# HEATING SYSTEM - TCH



1

## HEATING THE SOIL

Objective : Vaporise contaminants

2

## RECOVER CONTAMINANTS

Extract from soil all vaporised contaminants

3

## TREAT THE CONTAMINANTS

As fuel (in the burners) or  
as liquid product (after condensation)



# 2 Site description & Approach



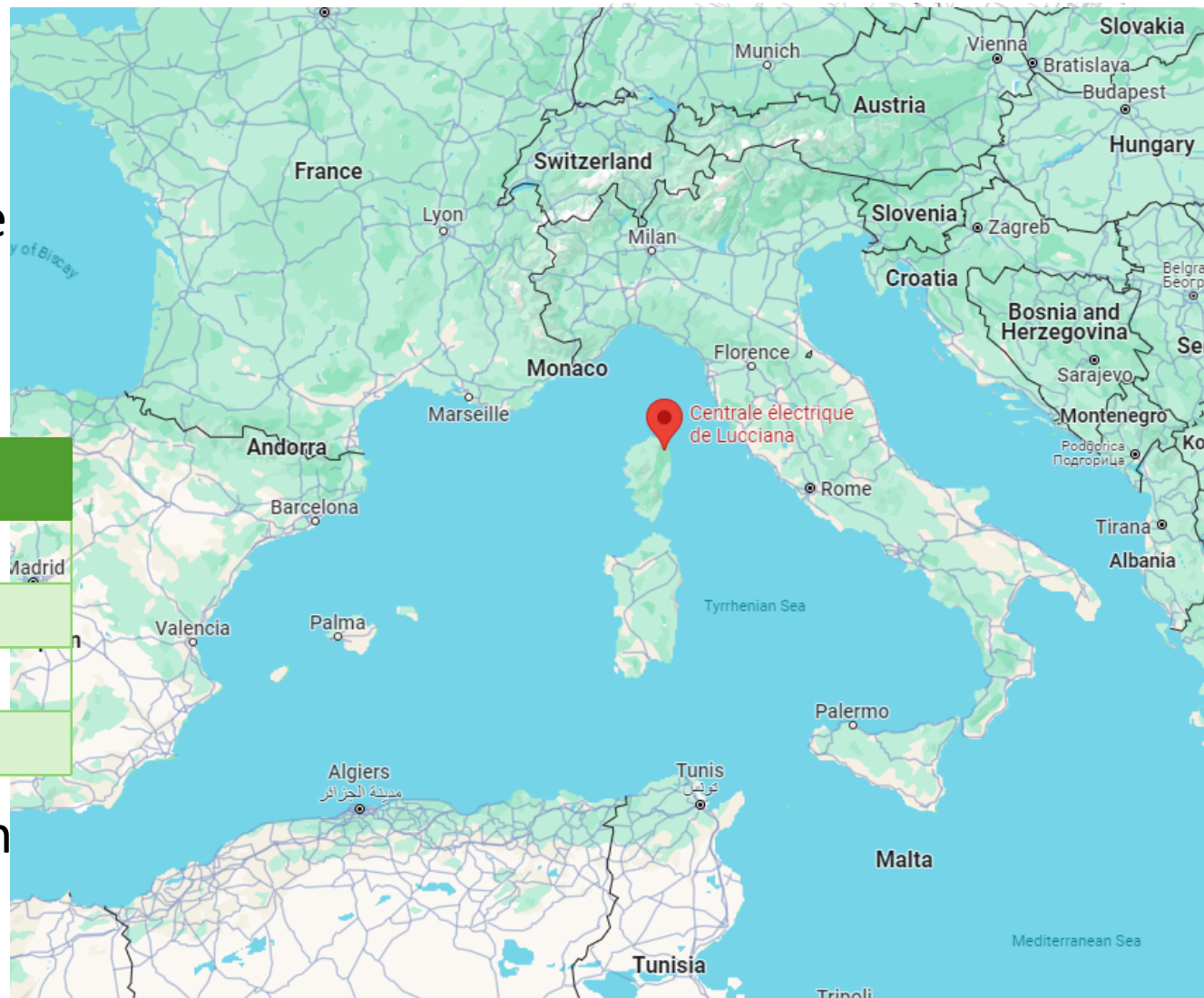
# Site description & stakeholders



- Client: EDF (Electricité de France)
- Site characterization: 2 impacted area in soil gas ( $> 20,000 \mu\text{g}/\text{yd}^3$ )  
VHOC contamination (up to  $730,000 \mu\text{g}/\text{yd}^3$ )  
1,1-DCA and  $340,000 \mu\text{g}/\text{yd}^3$  of 1,1,1-TCA)

| Description        | Quantity | Unit            |
|--------------------|----------|-----------------|
| GW Depth           | > 50     | ft              |
| Upper depth (ISTD) | 16       | ft              |
| Lower depth (ISTD) | 43       | ft              |
| Area               | 43,000   | ft <sup>2</sup> |

- Lithology : Sand/silty/clayey soil with multi-decimeter bloc



# Multi Approach Design

- Soil Gas Treatment (vadose area)

In-Situ TCH for hot spot ( $> 80,000 \mu\text{g}/\text{yd}^3$ )

Venting for peripheral zone ( $20,000 - 80,000 \mu\text{g}/\text{yd}^3$ )

- Groundwater Treatment (saturated area)

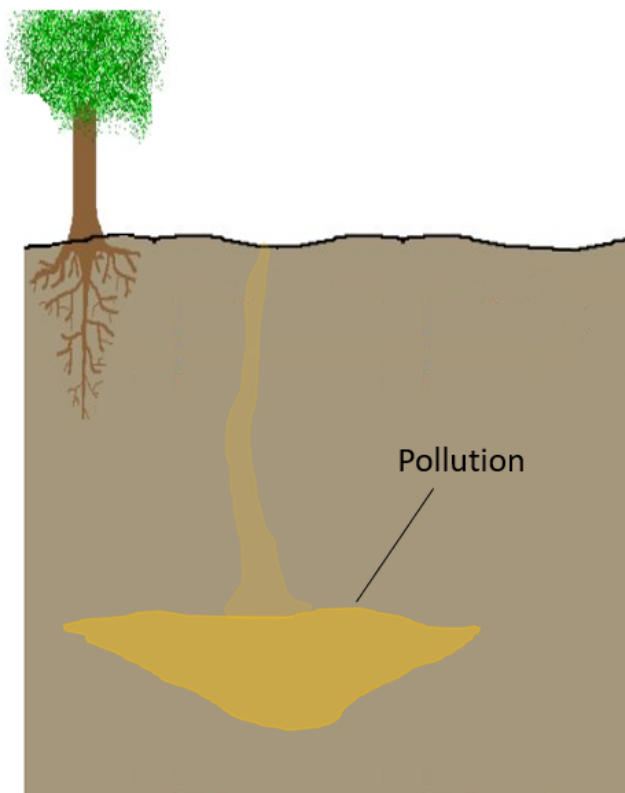
Pump & treat (collect of pure product and lowering groundwater)

Sparging

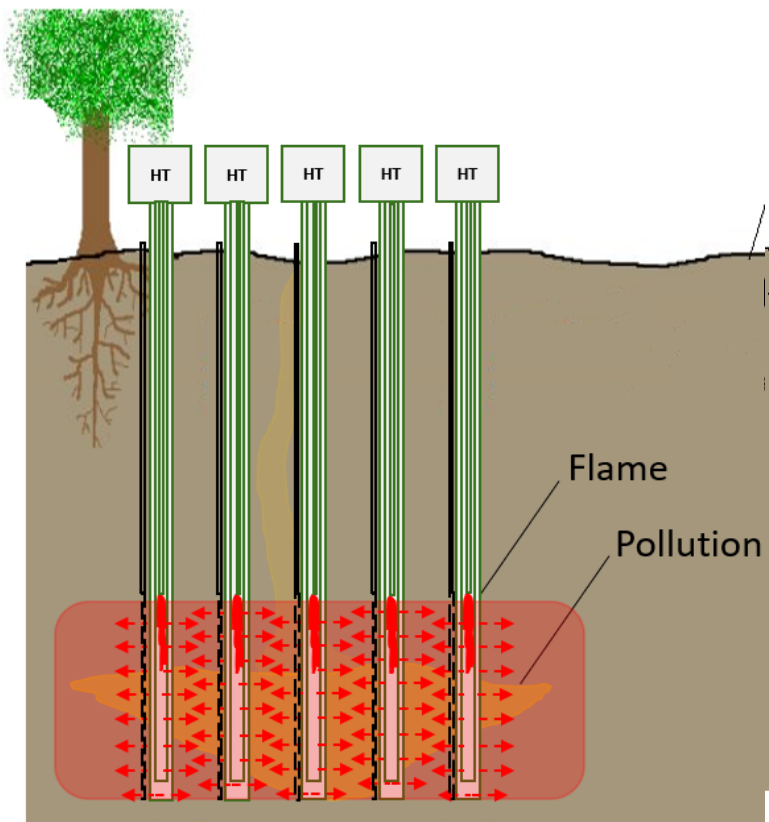
In-Situ Chemical Oxidation after total treatment



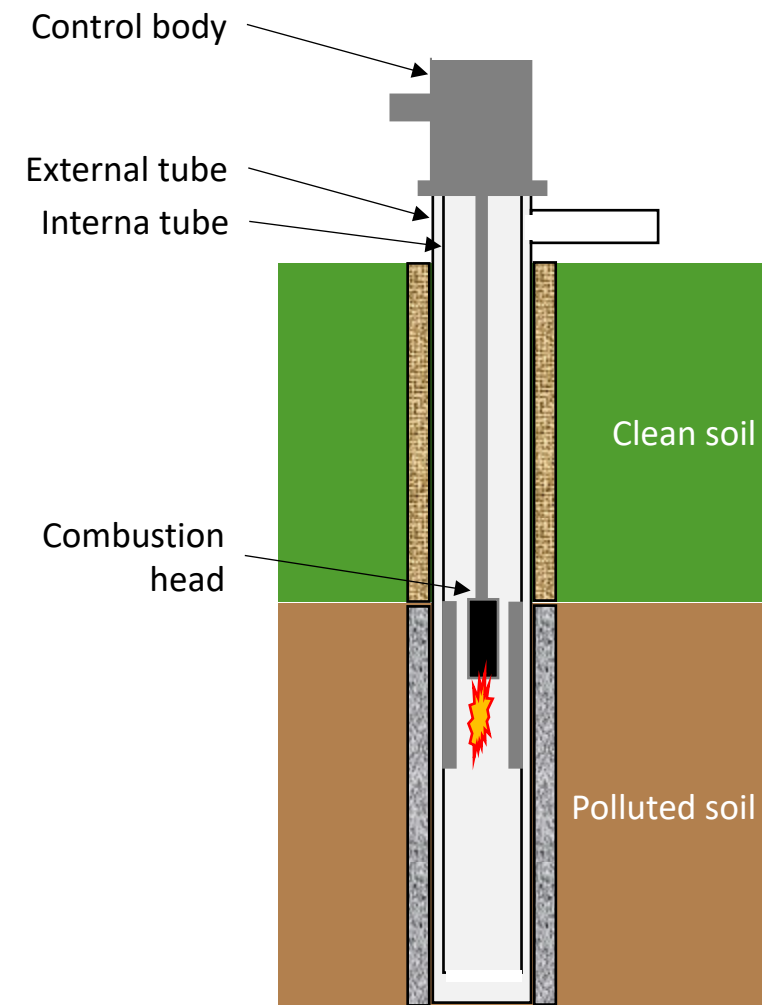
# In-Situ TCH – Remote flame technology



Without remediation



With Remote flame technology





3

## TCH design and results



# Batch 1 – Design & fuel consumption

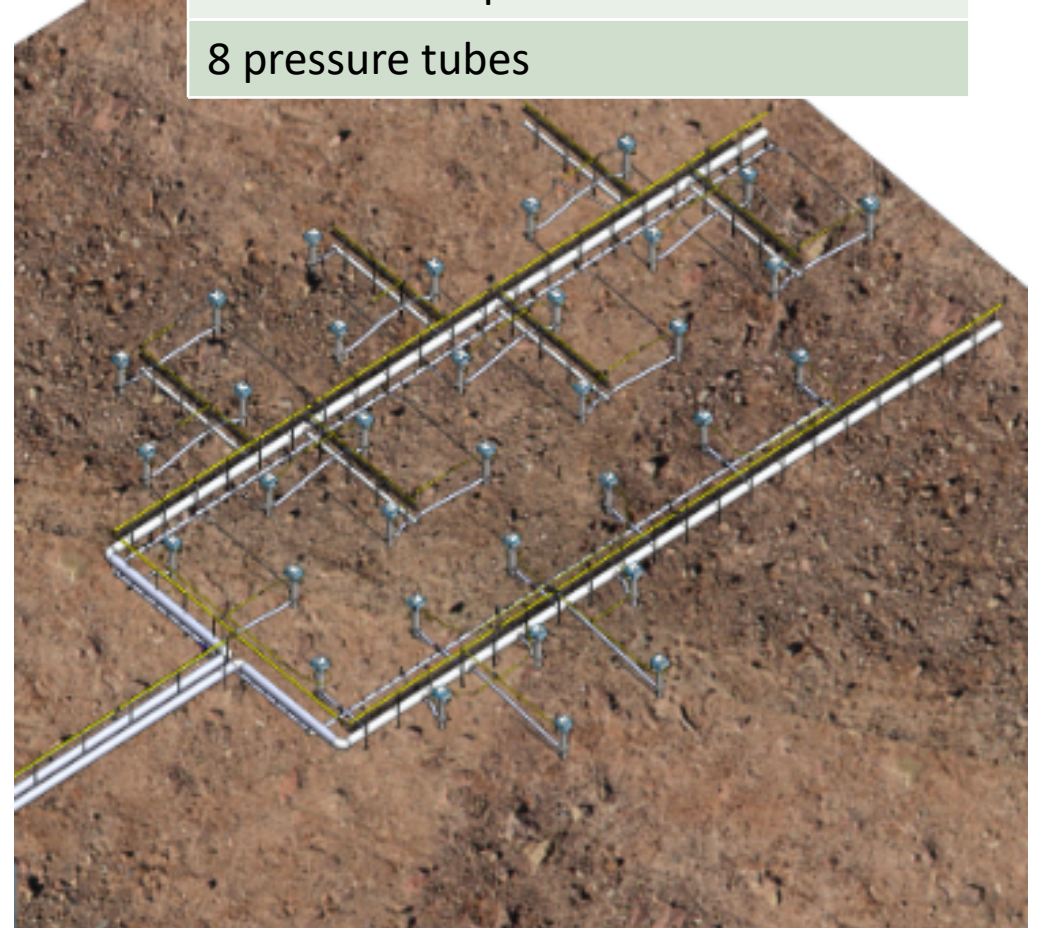


## Description

36 remote flame burners

15 thermocouples tubes

8 pressure tubes



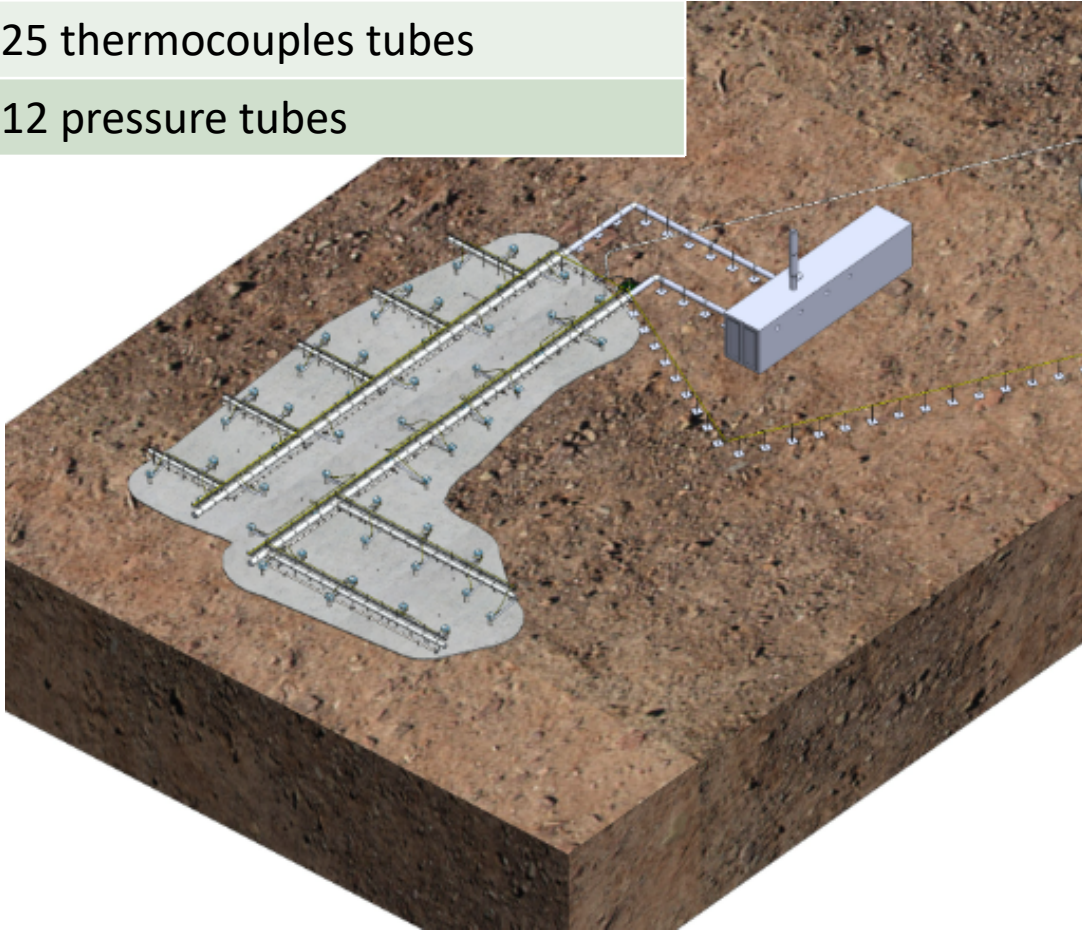
# Batch 2 – Design & fuel consumption

## Description

51 remote flame burners

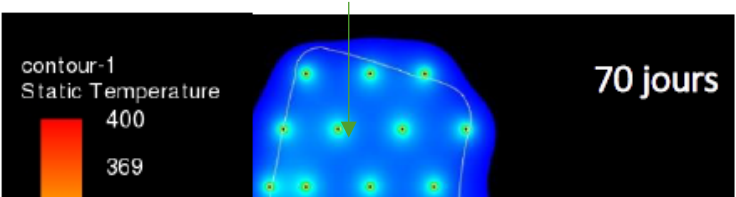
25 thermocouples tubes

12 pressure tubes

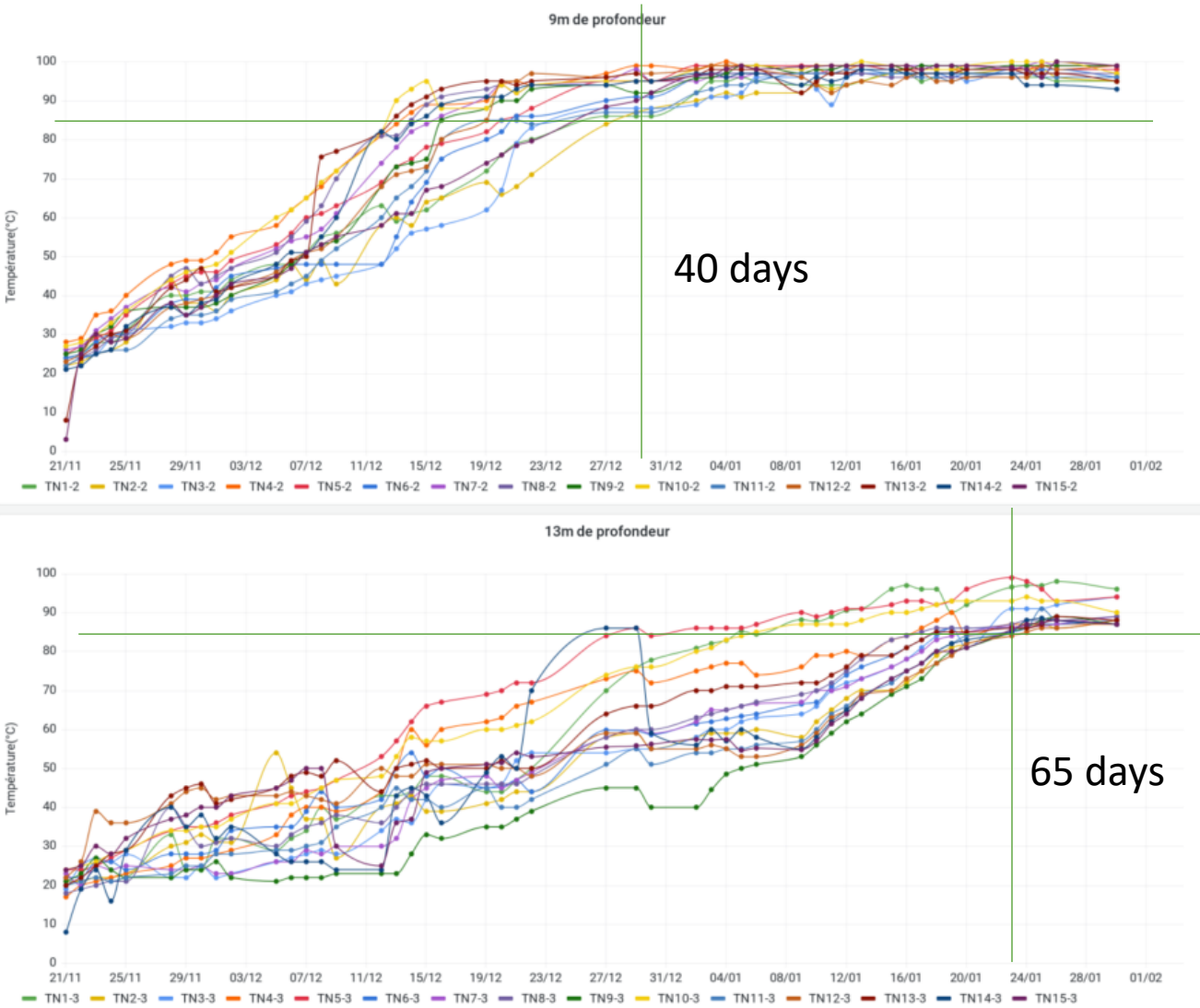
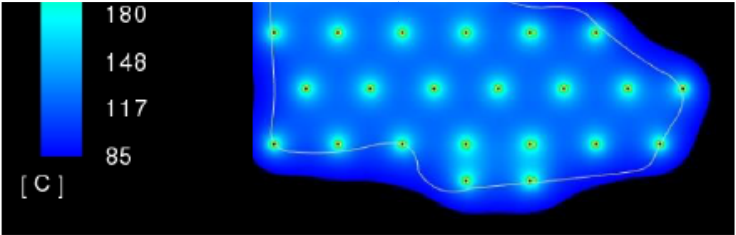


# In-Situ TCH – Heating phase

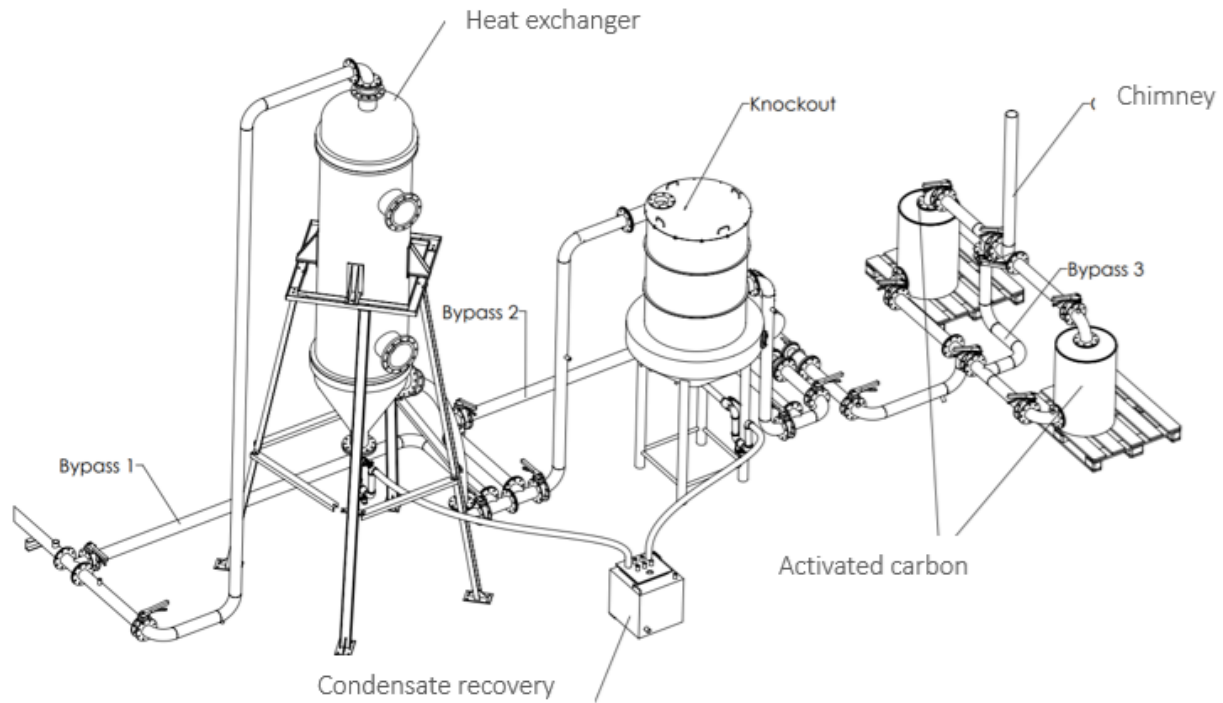
| Description       | Qtt                 |
|-------------------|---------------------|
| Target kinetic    | 85°C – 5 days at TT |
| Fluent Simulation | 70 days             |



| Description | Qtt                 |
|-------------|---------------------|
| North Area  | 74 days – 130 kWh/t |
| South Area  | 75 days – 115 kWh/t |

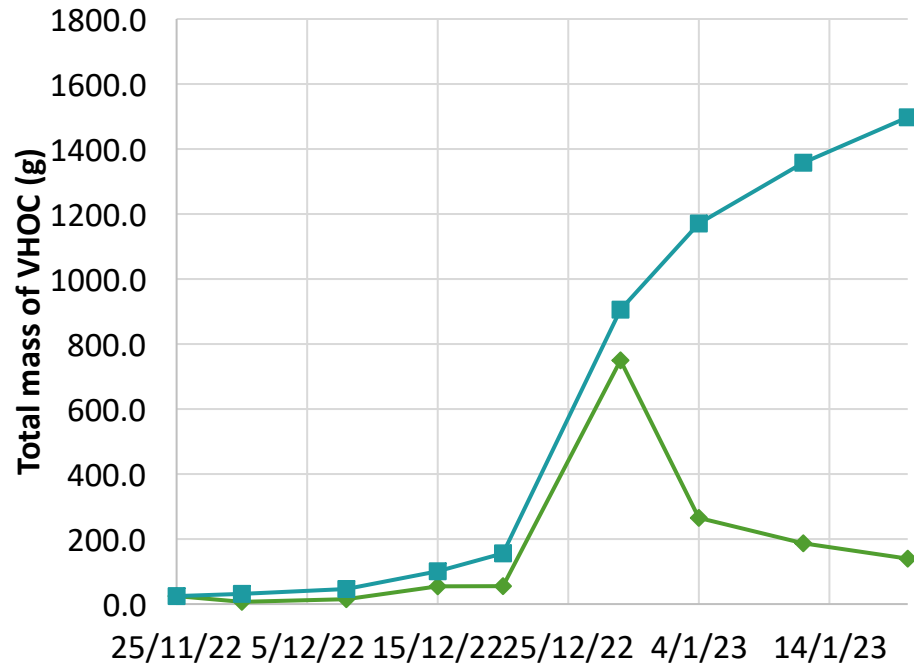


# Design – Vapor Treatment Unit



# Results

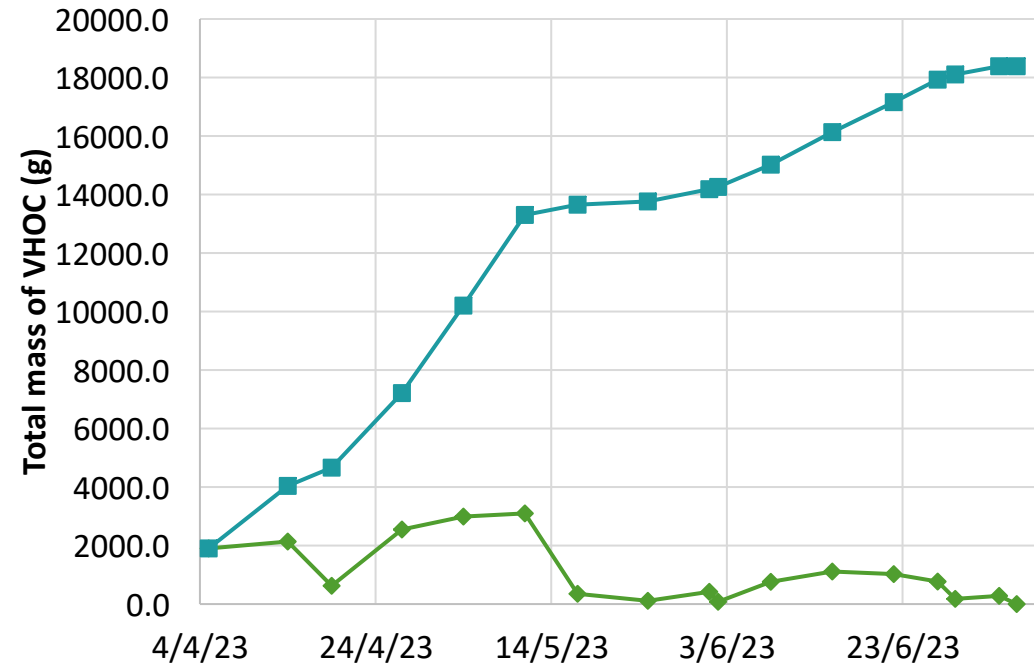
Batch 1



Final average  
concentration

25  $\mu\text{g}/\text{yd}^3$

Batch 2



Final average  
concentration

1,500  $\mu\text{g}/\text{yd}^3$

# Synergies with TCH

- Improved the efficiency of the venting at the boundaries
- Improved the efficiency of the chemical oxidation (injection at 40°C)



# 4 Conclusion



# CONCLUSION

- Complex site
- Multi technology approach
- TCH as backbone (synergies with venting and chemical oxidation)
- Scalable and predictable technology (70 days in the simulation and during operations)
- Low recovery mass in the VTU due to the presence of venting VTU



Thank you for your attention !

