

Regenerable Ion Exchange Treatment with Hydrothermal Alkaline Treatment (HALT): Full Spectrum PFAS Capture and Destruction

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¹Emerging Compounds Treatment Technologies, Inc., ²Aquagga, Inc.

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Acknowledgments

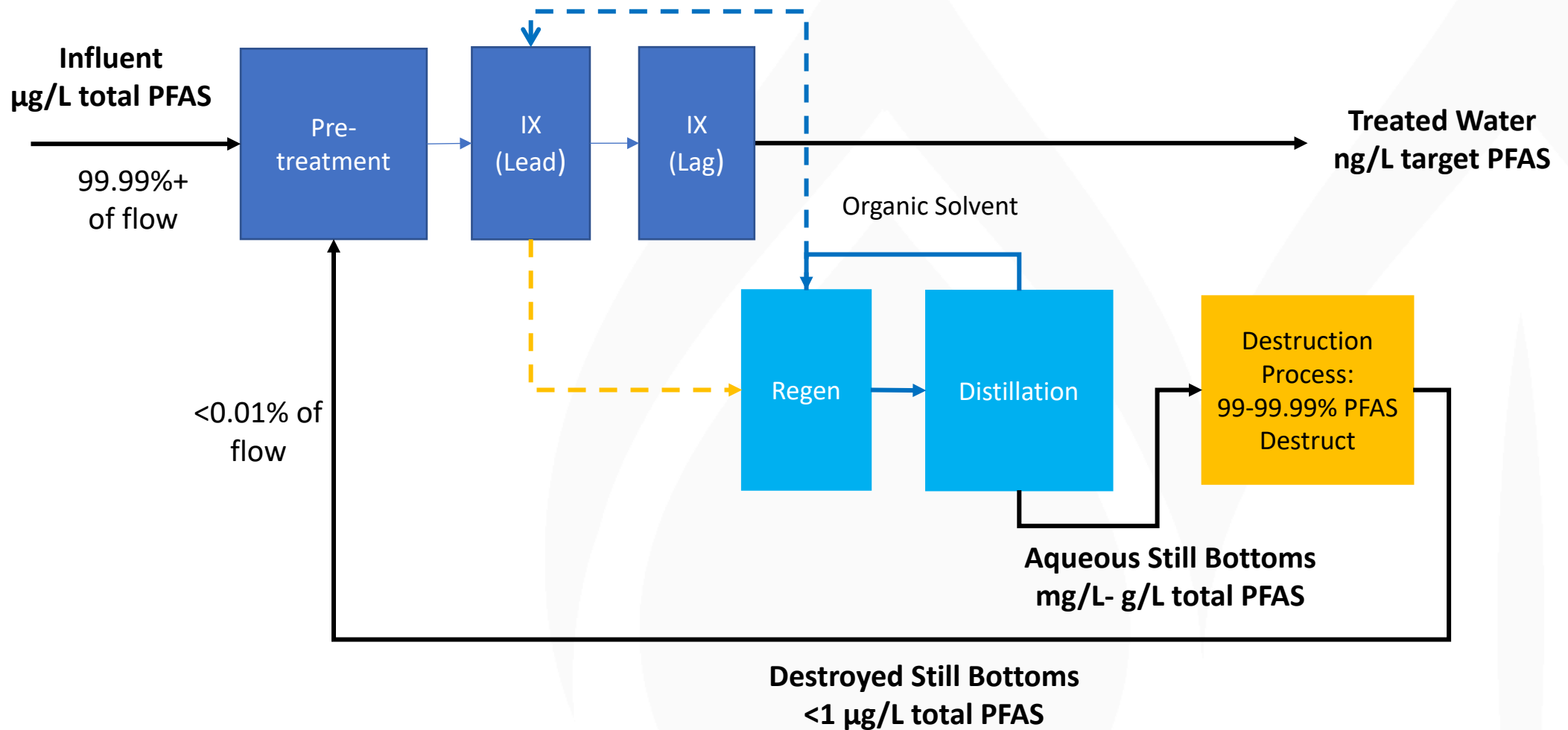
- Hunter Anderson at AFCEC
- Aquagga Collaborators (Brian Pinkard, Gus Millevolte, Conrad Austin)
- ECT2 Colleagues (Steve Woodard, Mike Nickelsen, John Berry, Dave Kempisty, Jess Haxon, Cameron McClellan, J Esteves)



Key Messages

- Regen IX is a good fit for high conc PFAS influent and/or short chain PFAS removal
- Regen IX creates a PFAS concentrate (“still bottoms”) amenable to destruction
- Hydrothermal alkaline treatment (HALT) is robust in the still bottoms matrix
- Full spectrum PFAS destruction with mineralization observed with HALT
- HALT conditions can be optimized to 99.9%+ destruction efficiency
- Regen IX and HALT can be paired to create a closed loop treatment process

Regen IX Process with Destruction Incorporated



Still Bottoms: End product of the regen IX process

Relevant Characteristics:

- 2%+ NaCl
- ~0.1 to 5 g/L total PFAS
- Color
- Inorganic ions (nitrate, sulfate)
- Neutral to basic pH
- Trace solvent



ECT2 Full Scale Regen IX System Images

Complete System
Aerial in Australia



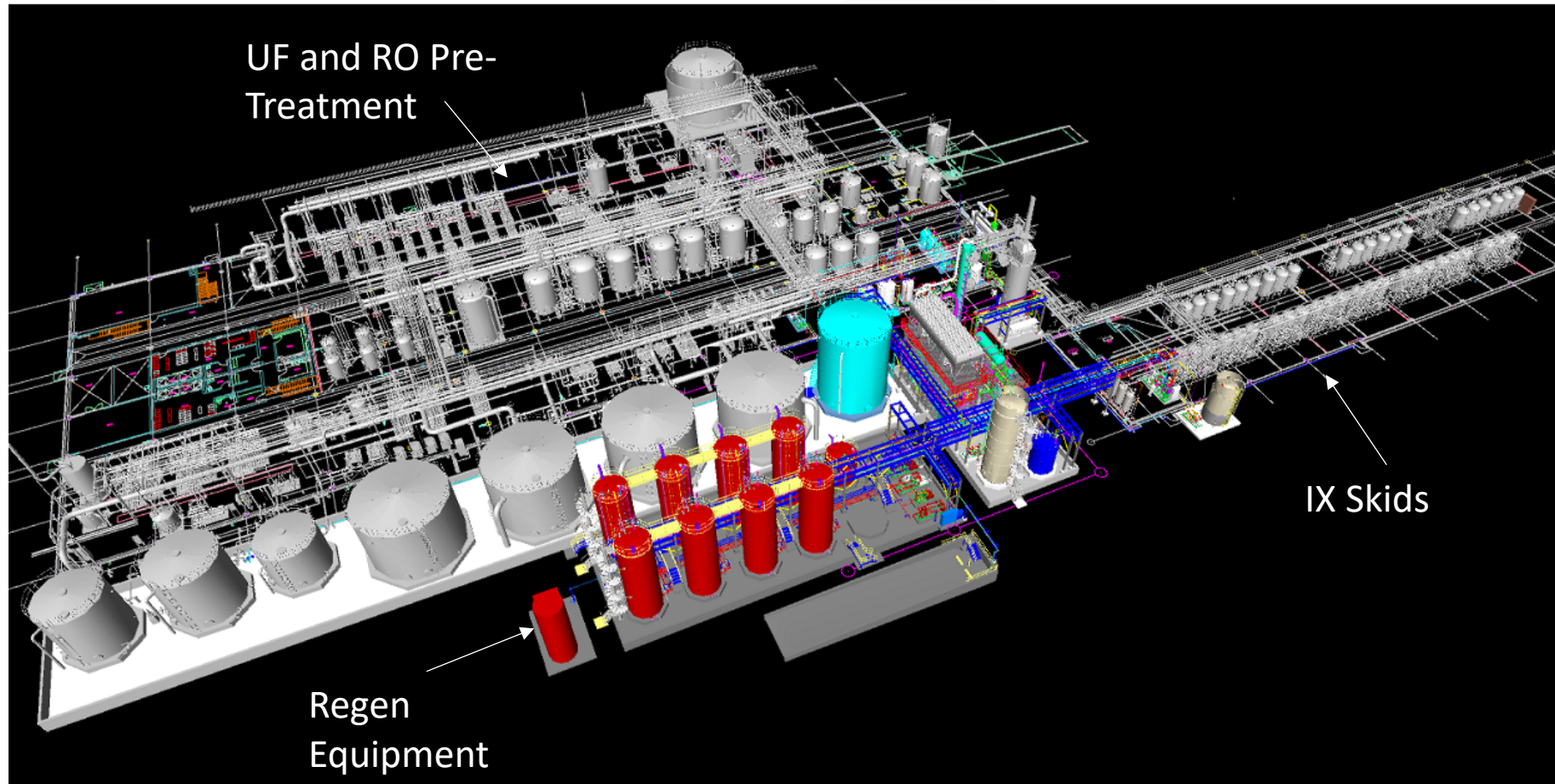
Resin
Vessels



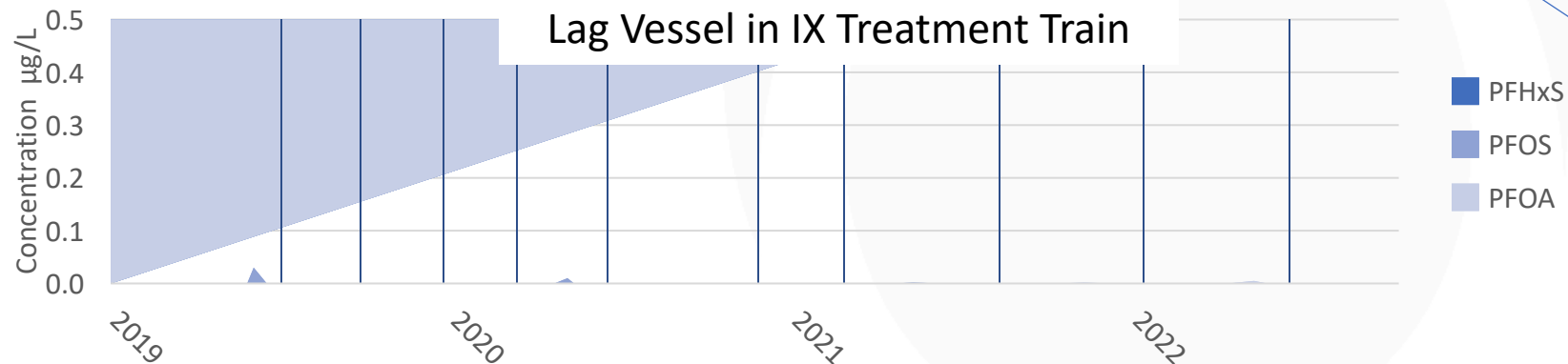
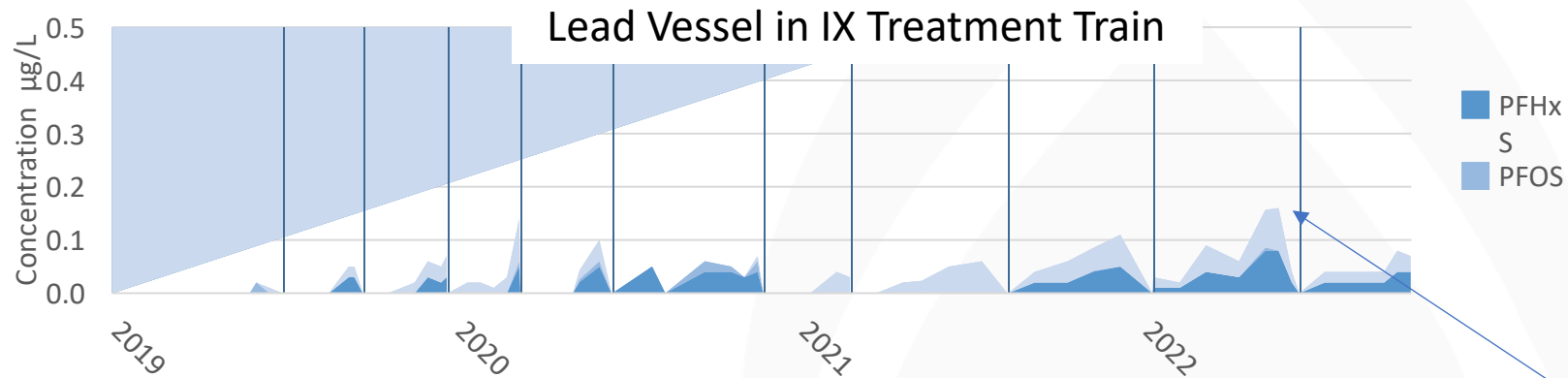
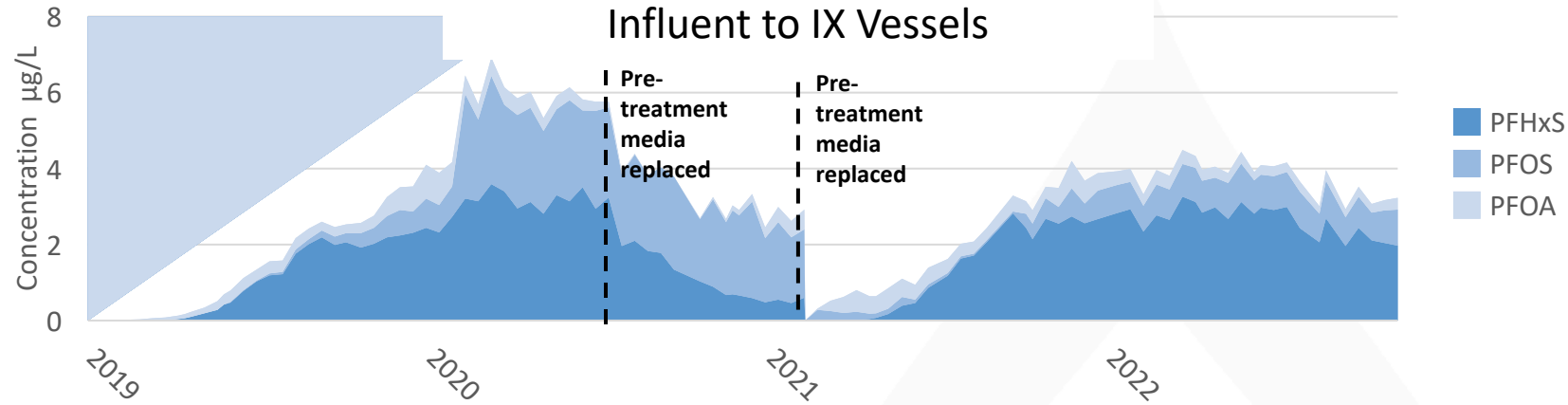
Distillation
Equipment



Overview of an 8000 gpm Regen IX Plant Designed for Industrial Client



Continuous Regen IX Performance Over Four Years of Operation



Across 4 years of regeneration cycles, the IX resin continues to achieve PFAS treatment objectives with no degradation in performance

Vertical lines indicate resin regeneration in lead vessel (triggered by exceedance of 70 ppt PFOS + PFHxS in lead vessel effluent); vessels rotated following regen

Fate of Still Bottoms

- At most ECT2 regen IX systems, still bottoms are Superloaded onto mixed media
 - Overall concentration factors of 1 million + ($V_{\text{water treated}} / V_{\text{Disposed Superloader media}}$)
 - Superloader media lasts years without replenishment
- Still bottoms are also a prime candidate for PFAS destruction
 - Low volume - 10,000x+ concentration factor ($V_{\text{water treated}} / V_{\text{Still Bottoms}}$)
 - High concentration (mg/l to g/l total PFAS)

Superloader vessels for a 200 gpm system



Still Bottoms can be Superloaded onto media or destroyed with a process such as HALT

Hydrothermal Alkaline Treatment (HALT)

- Developed at Colorado School of Mines; offered commercially by Aquagga
- Barely subcritical treatment - high pressure, high temperature, high pH (350°C, >20.7 MPa, pH>14)
- Destruction reaction with PFAS is driven by a nucleophilic reaction with hydroxide; thermal degradation also occurs
- Residence times ~ minutes
- pH adjustment occurs at end of reaction

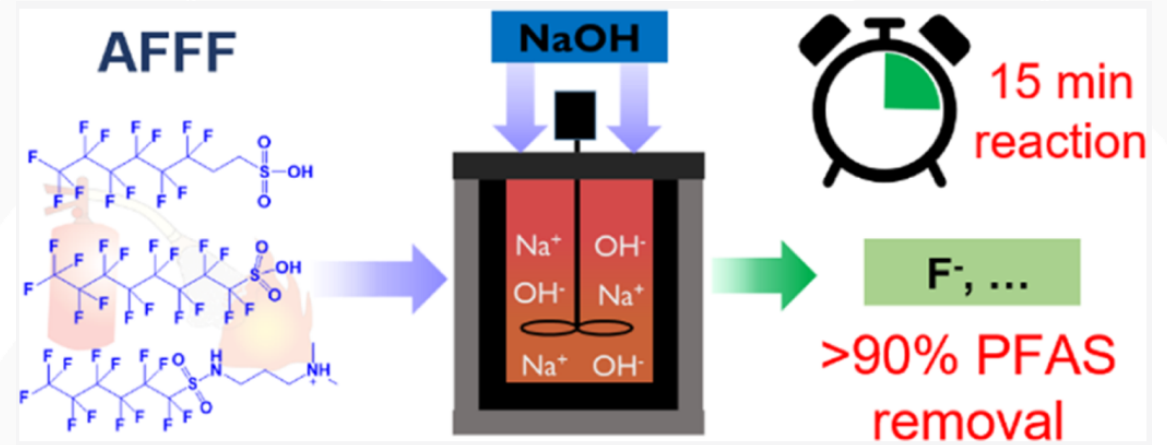


Image from Hao et al 2021

Aquagga HALT Test Plan

- ECT2 collected still bottoms from a US DoD site in Spring 2023
- Multiple additional PFAS spiked at 25 mg/l
 - Another subset was additionally spiked with additional salts to simulate RO-treatment and desorption of common anions
- Aquagga conducted testing in two phases in the 1 gph pilot unit:
 - Compared treatment of RO-still bottoms to typical still bottoms
 - Optimized for NaOH concentration
 - Optimized for temperature



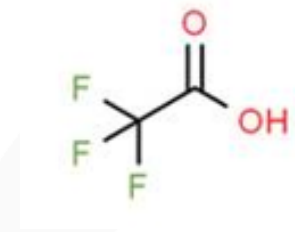
Salt, mg/L	Still Bottoms	RO Still Bottoms
NaCl	27,000	60,000
Na ₂ SO ₄	4,800	6,000
NaNO ₃	8,000	20,000

Testing Goals: Optimize Still Bottoms Treatment with HALT + Close F Mass Balance

Aquagga HALT Test Plan

- Untreated and treated samples analyzed at Enthalpy Analytical for:
 - 533 PFAS analyte list
 - Polar PFAS analyte list
 - Fluoride
 - Adsorbable organofluorine (AOF) – EPA Method 1621
 - Gas phase: FTIR (at ECT2 R&D lab)

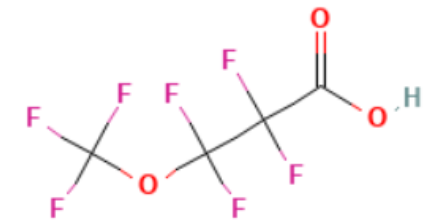
TFA



PFEESA



PFMoPrA



Testing Goals: Optimize Still Bottoms Treatment with HALT + Close F Mass Balance

Percentage Destruction by Analyte

	Initial Concentration After PFAS Additions (ppb)	Test 1.1 Level 3 NaOH Design Temp; Very high salt	Test 1.2 Level 4 NaOH Design Temp; Very high salt	Test 1.3 Level 3 NaOH Design Temp	Test 1.4 Level 4 NaOH Design Temp	Test 2.1 Level 2 NaOH Design Temp + 25	Test 2.2 Level 5 NaOH Design Temp + 25	Test 2.3 Level 2 NaOH Design Temp + 35	Test 2.4 Level 1 NaOH Design Temp + 35
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PFPrA	16,200	99.90%	99.89%	99.980%	99.940%	99.810%	99.790%	99.801%	99.826%
PFBA	34,000	99.99%	99.98%	99.990%	99.985%	99.998%	99.998%	99.998%	99.998%
PFPeA	4,870	99.96%	99.96%	99.970%	99.954%	99.990%	99.989%	99.989%	99.991%
PFHxA	14,700	99.98%	99.98%	99.983%	99.974%	99.996%	99.996%	99.996%	99.996%
PFHpA	2,910	99.91%	99.91%	99.926%	99.913%	99.979%	99.977%	99.978%	99.981%
PFOA	35,100	99.95%	99.99%	99.961%	99.961%	99.999%	99.999%	99.999%	99.999%
TFMS	22,200	85.20%	85.69%	96.531%	97.100%	97.865%	99.489%	99.793%	99.819%
PFBS	30,400	92.10%	95.13%	95.249%	95.023%	98.744%	99.783%	99.978%	99.901%
PFPeS	1,340	91.24%	95.91%	95.225%	94.111%	98.972%	99.807%	99.963%	99.887%
PFHxS	38,000	--	94.63%	92.107%	80.424%	99.201%	99.774%	99.962%	99.736%
PFOS	12,200	--	97.47%	75.056%	72.239%	99.843%	99.793%	99.865%	99.247%
6:2 FTS	28,900	98.95%	98.90%	98.972%	98.424%	99.987%	99.997%	99.997%	99.997%
HFPO-DA	37,400	99.99%	99.99%	99.993%	99.990%	100.000%	99.999%	99.999%	100.000 %
PFMOPrA	33,300	99.99%	99.99%	99.989%	99.986%	99.998%	99.998%	99.998%	99.998%
PFEESA	35,400	84.27%	90.89%	90.963%	89.503%	98.726%	99.523%	99.938%	99.776%
AOF	121,260	--	--	--	--	98.542%	99.843%	99.843%	99.843%

Blue cells were non-detect in treated solutions and represent minimum percentage destruction

99% to 99.99% Destruction Across All PFAS Under Optimized Conditions

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PFCAs,
Fluorotelomers, and
perfluoroalkyl
carboxylic ethers
completely destroyed
under all test
conditions

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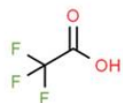
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PFSA destruction percentages were largely independent of chain length

Perfluoroalkyl ether sulfonate had similar recalcitrance as PFSAs



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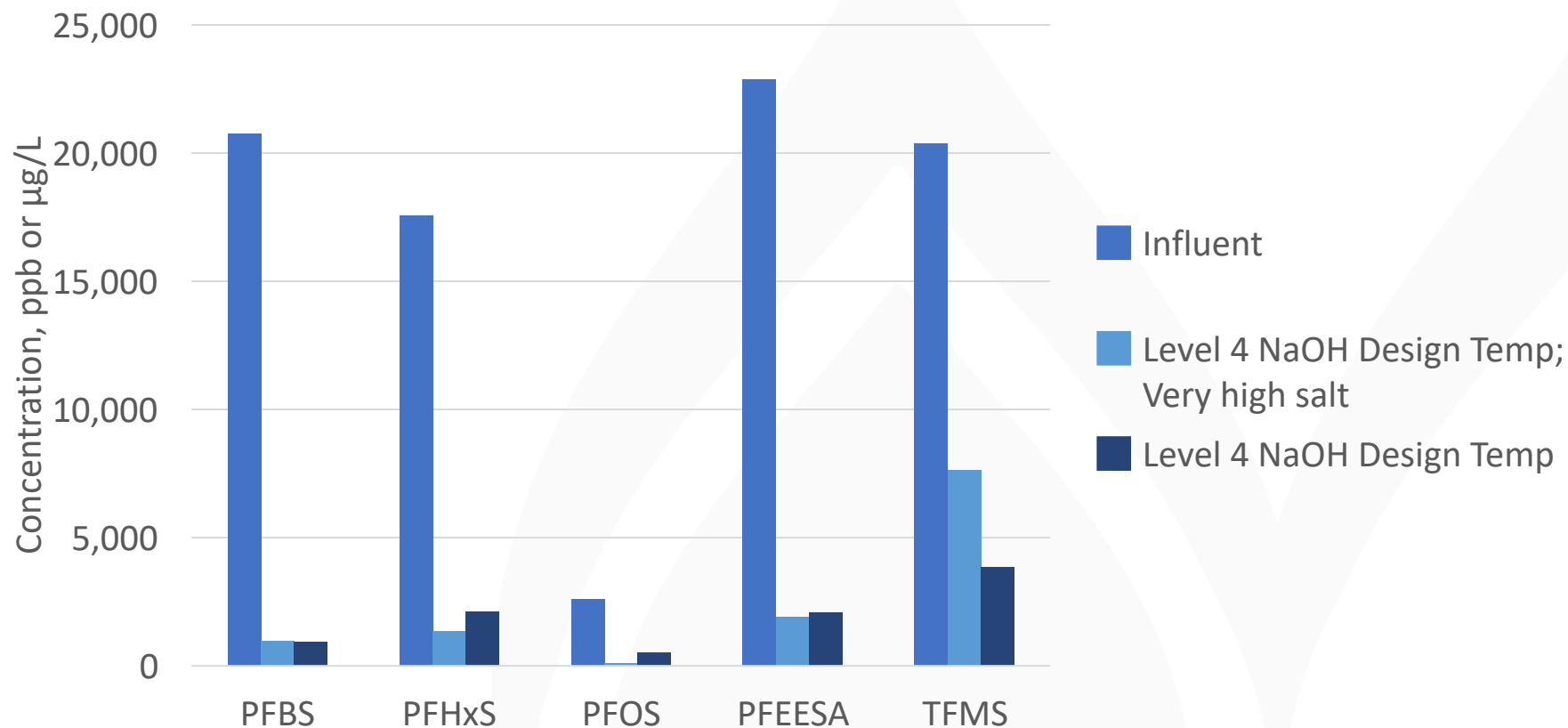
Excellent destruction
of ultrashort PFAS,
including TFA and
TFMS

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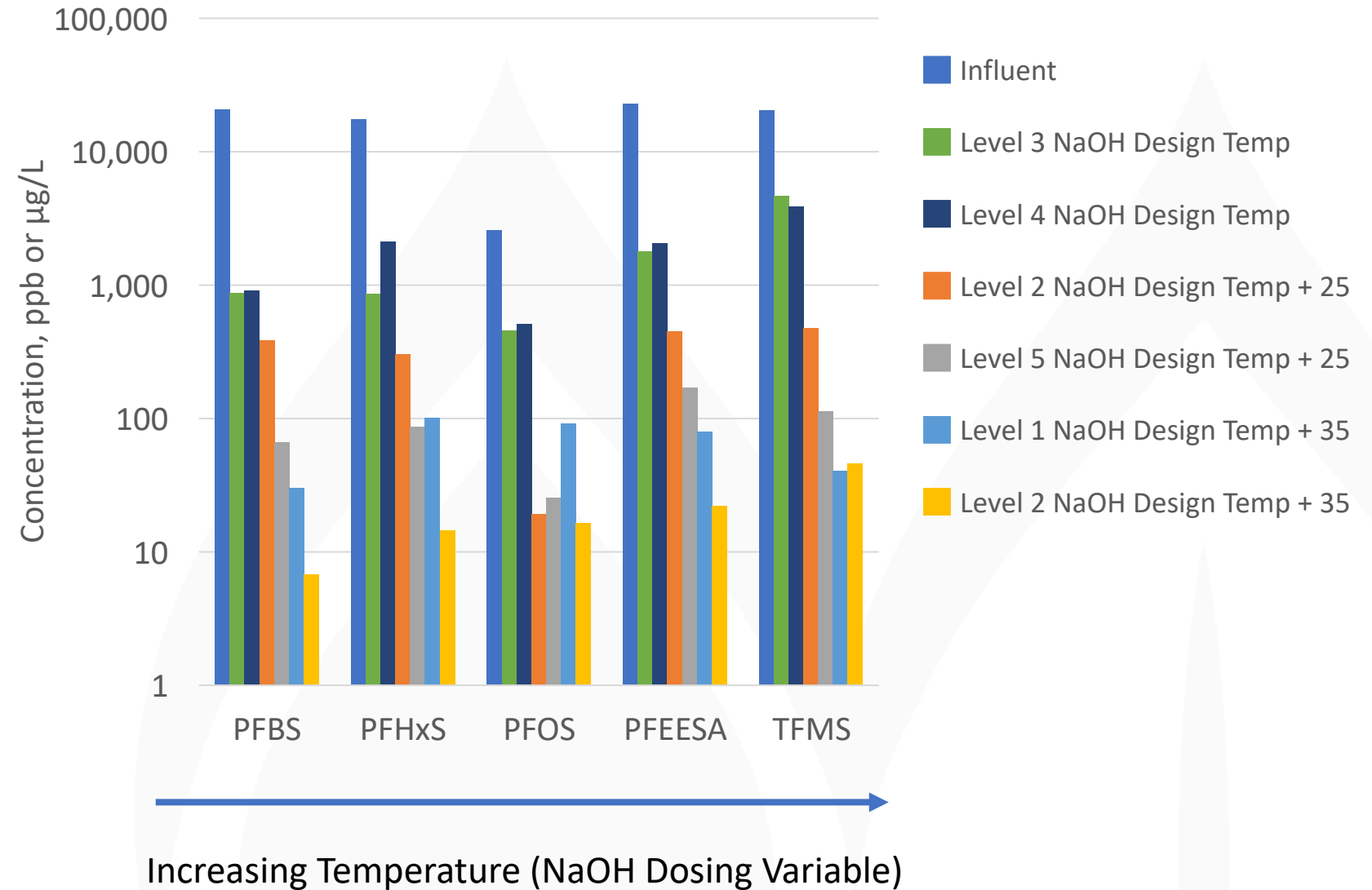
99.8%+ destruction of
AOF – line of evidence
for mineralization

HALT Testing: RO-Concentrated Still Bottoms vs Regular Still Bottoms



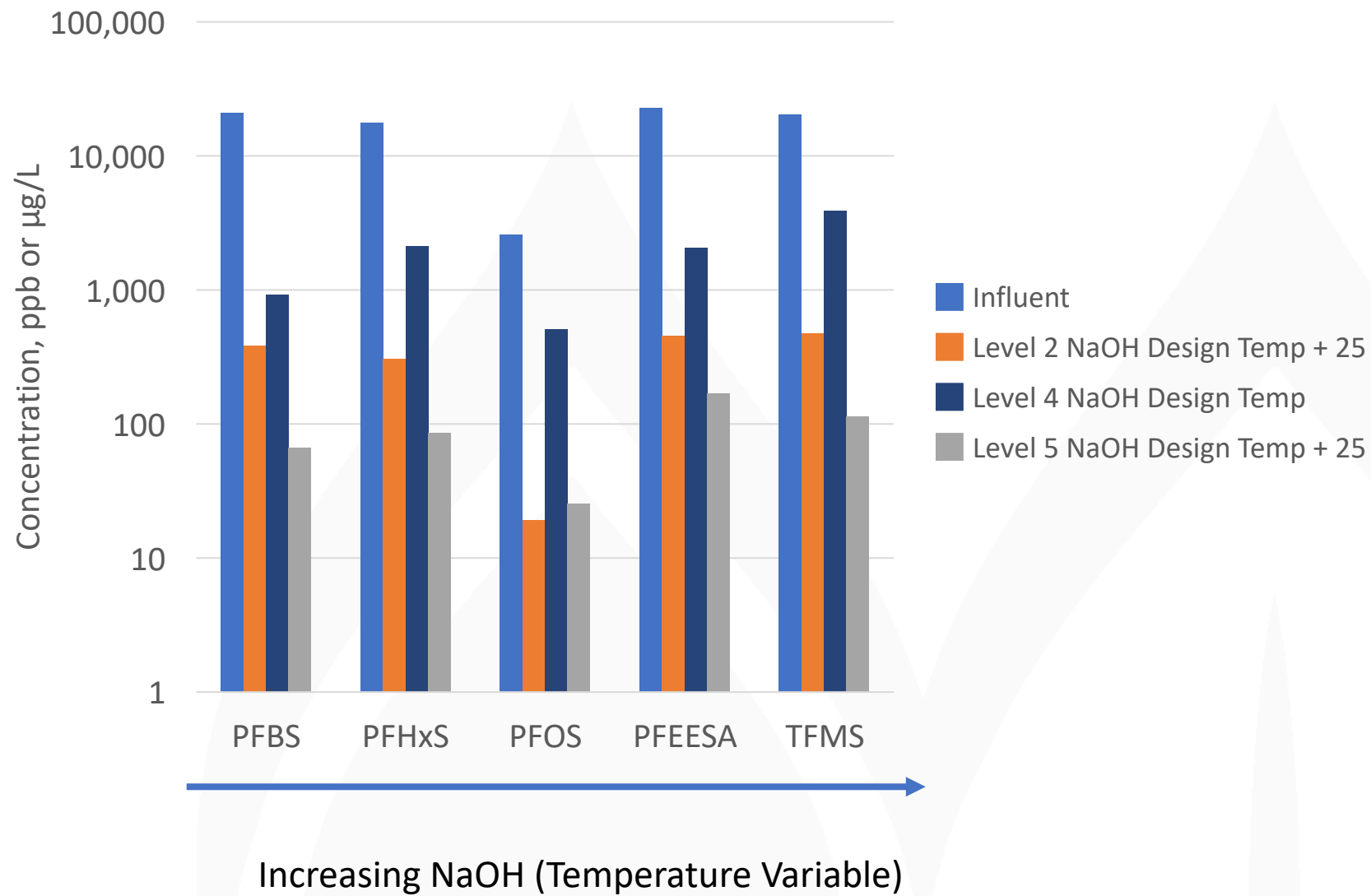
Simulated RO-Concentrated Still Bottoms Matrix Did Not Adversely impact HALT

Variation in
Recalcitrant
Compounds
in Treated
Effluent



Increasing Design Temperature by 25 - 35 C Increased Destruction 90-99%

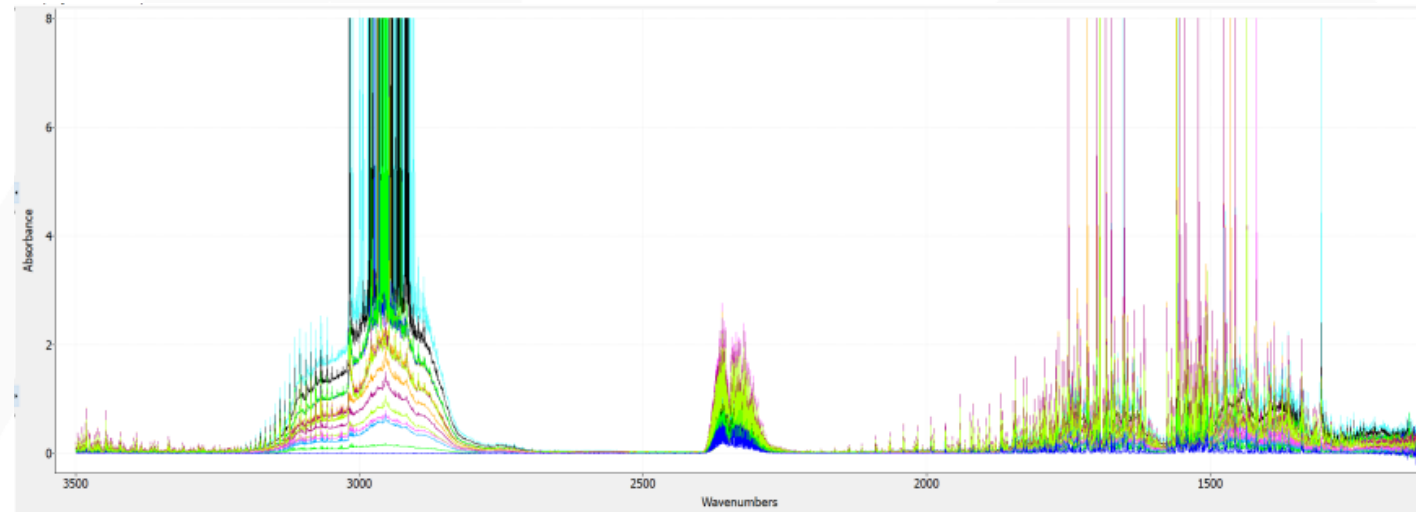
Variation in Recalcitrant Compounds in Treated Effluent



Increasing NaOH Dosage Was Less Impactful than Increasing Temperature

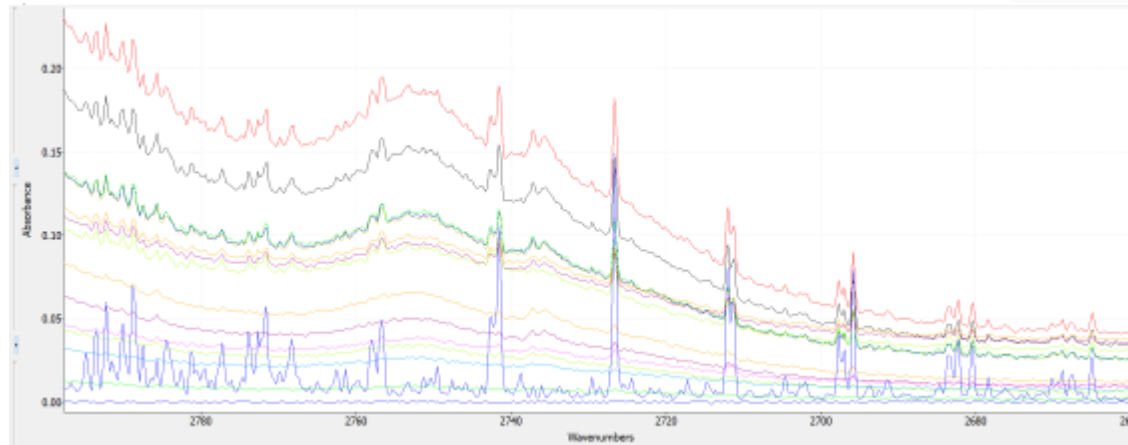
Qualitative FTIR Analysis of Offgas

- Three samples were analyzed by a Thermoelectrically cooled Fourier Transform Infrared Spectroscopy (FTIR)
- All three had similar spectra
- FTIR reference spectra used to evaluate the presence/ absence of various potential byproducts

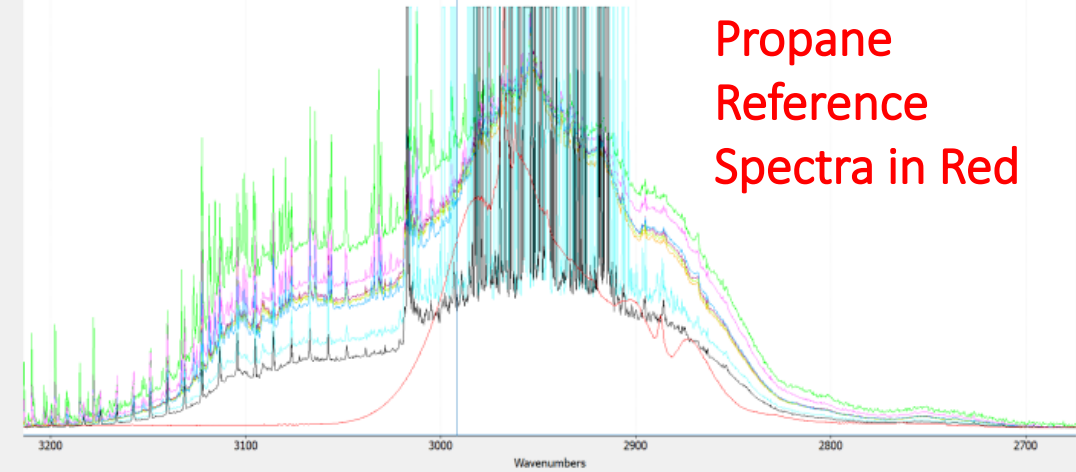


FTIR Analysis of Gas Effluent – Presence of Alkanes

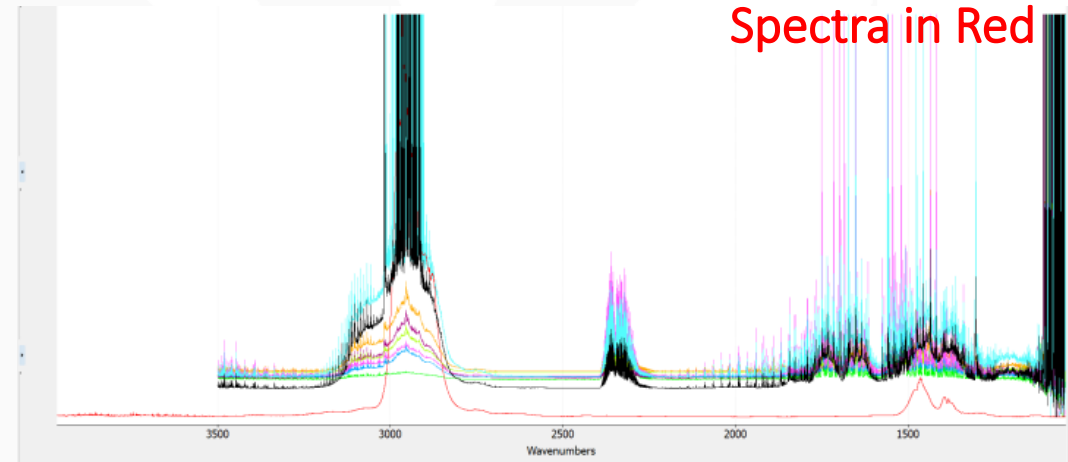
Methane Reference Spectra in Purple



Propane
Reference
Spectra in Red



Butane
Reference
Spectra in Red

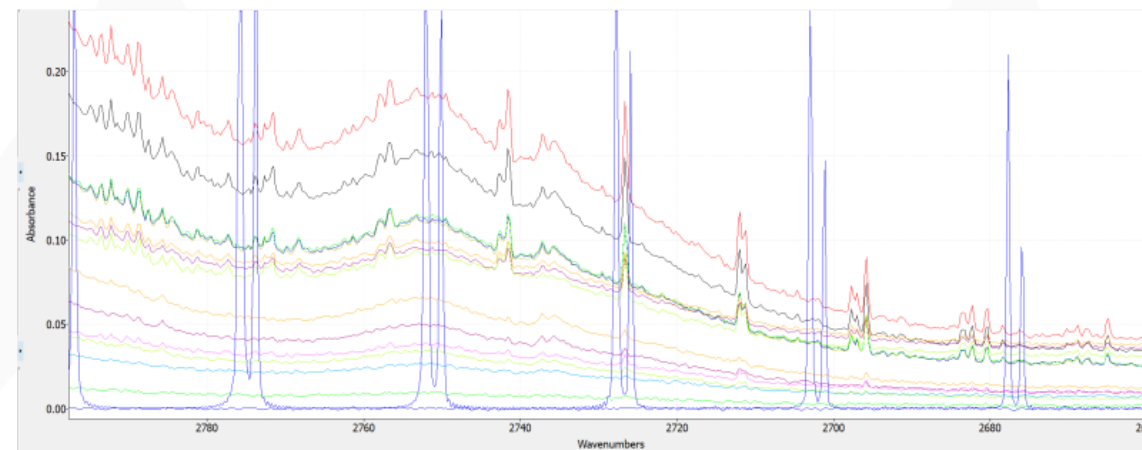


Significant reference spectra overlap indicates presence of methane, propane, butane

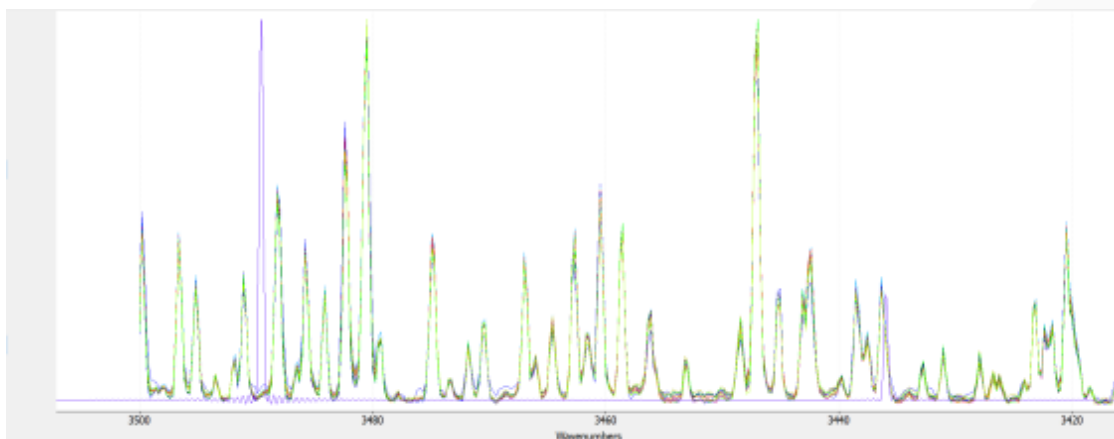
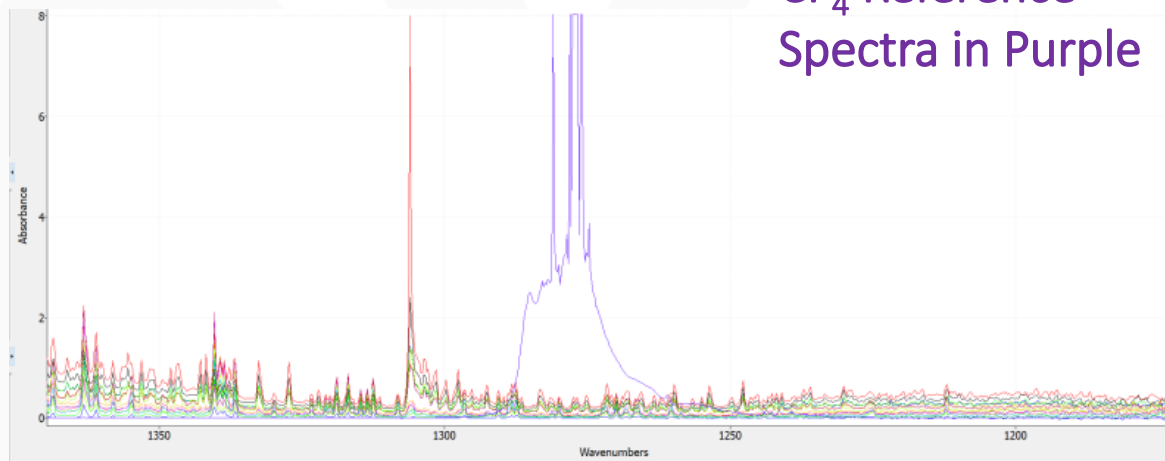
FTIR Analysis of Gas Effluent – Lack of HF, HCl, and CF₄

HCl Reference
Spectra in Purple

HF Reference
Spectra in Purple

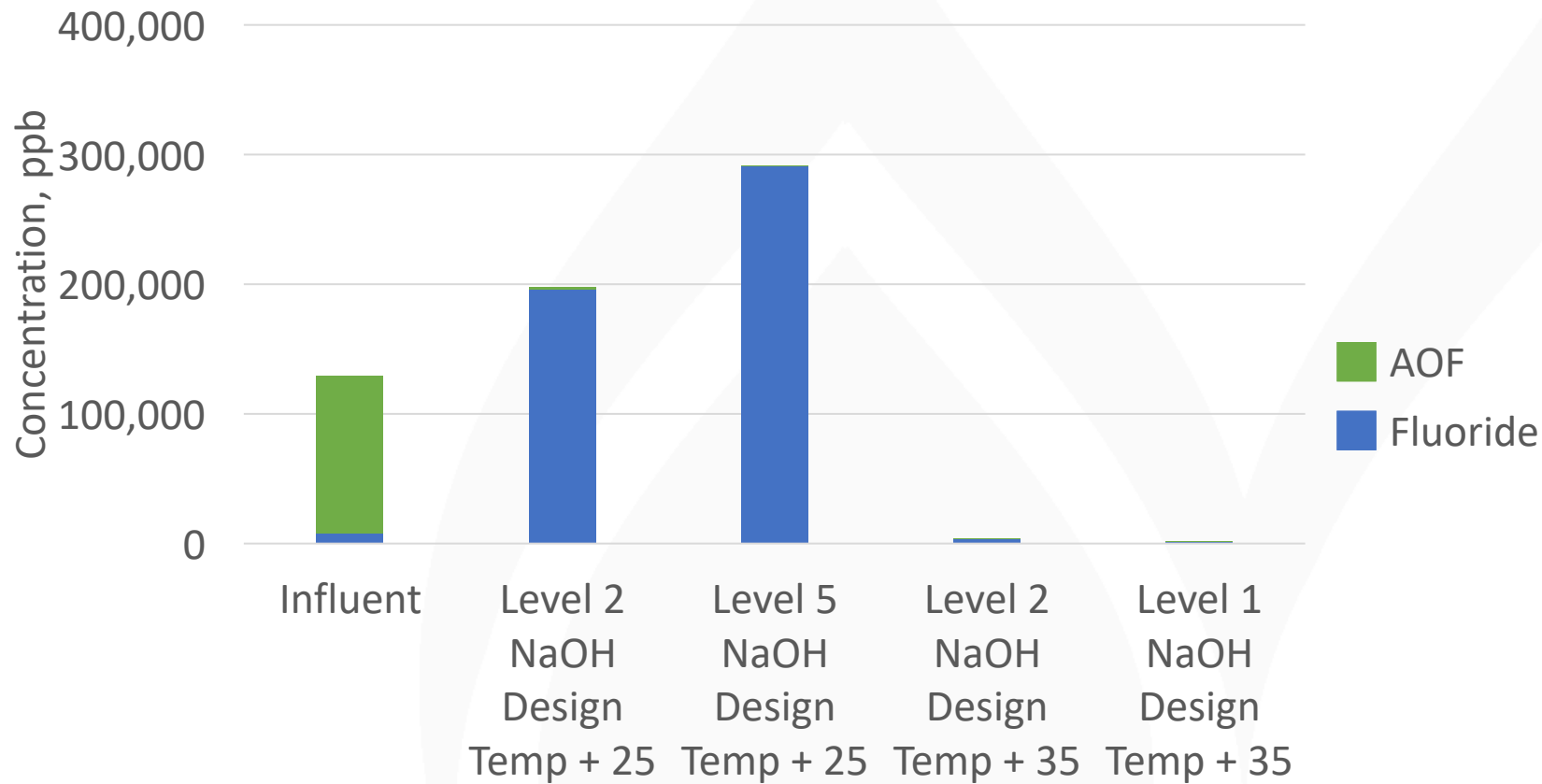


CF₄ Reference
Spectra in Purple



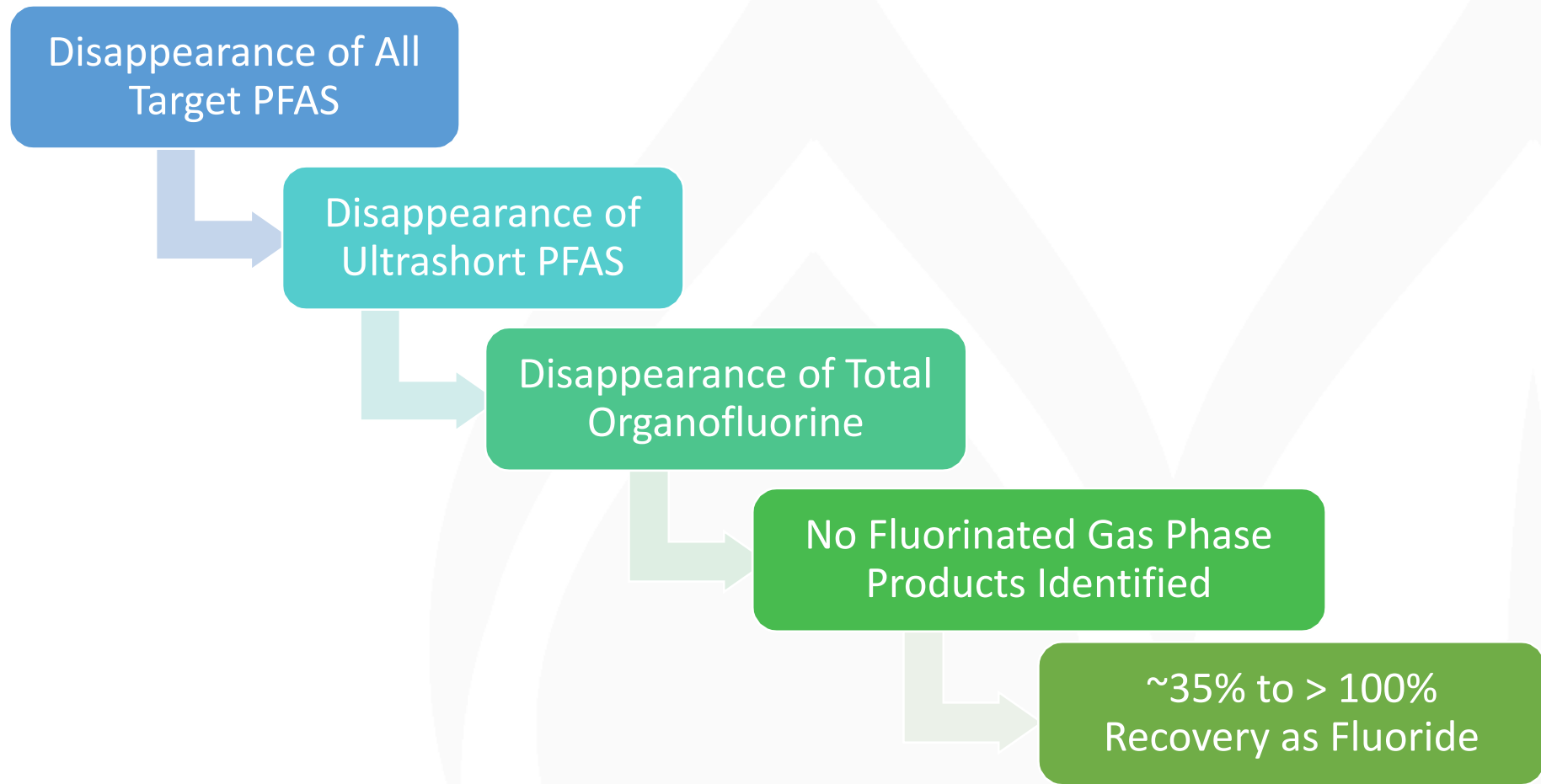
Lack of reference spectra overlap indicates lack of HCl, HF, and CF₄

Fluorine Mass Balance



Best Fluorine Mass Balance Observed at Design Temp + 25 C

Strong Evidence for PFAS Mineralization Using HALT on Still Bottoms



Key Messages

- Regen IX is a good fit for high conc PFAS influent and/or short chain PFAS removal
- Regen IX creates a PFAS concentrate (“still bottoms”) amenable to destruction
- Hydrothermal alkaline treatment (HALT) is robust in the still bottoms matrix
- Full spectrum PFAS destruction with mineralization observed with HALT
- HALT conditions can be optimized to 99.9%+ destruction efficiency
- Regen IX and HALT can be paired to create a closed loop treatment process